



COMSOL Multiphysics - fuel cell and LED applications

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Outline



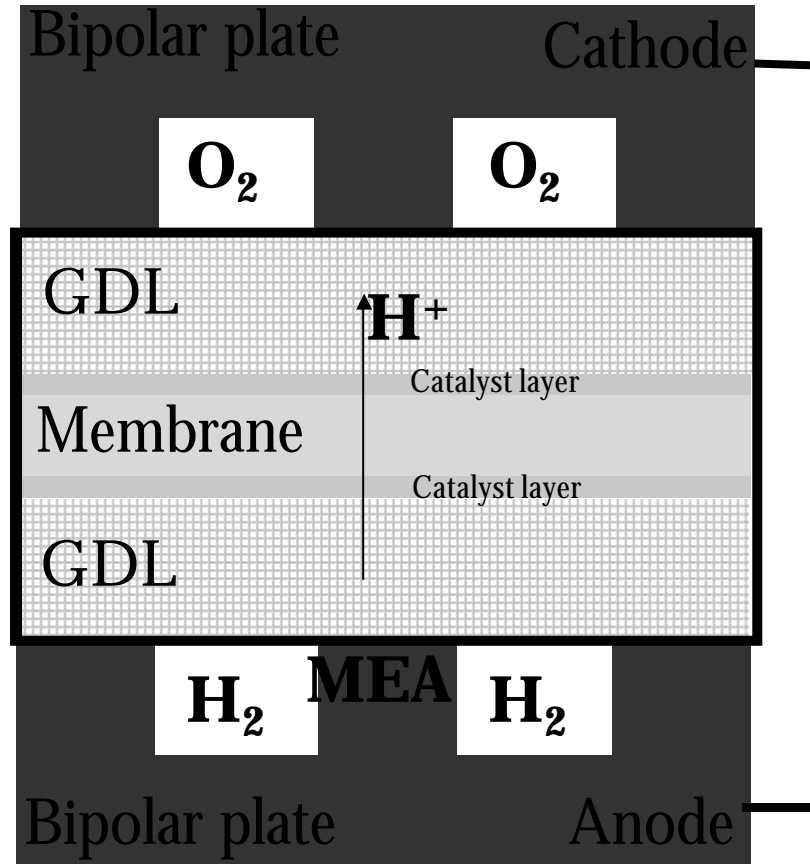
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- Introduction
- Simulation detail
- FC applications
 - 2D MEA model
 - 3D single cell model
 - FC Stack simulation
- LED applications
- Summary





How fuel cell works



• **Bipolar plate** (graphite): \sim 10000 μ m

electron conduction

• **Gas channel**: \sim 1000 μ m

gas transport

• **GDL** (Carbon cloth/paper): \sim 250 μ m
electron conduction and gas/water transport

• **CL** (Pt, Carbon, Nafion): \sim 10 μ m

electron conduction, gas/water transport
proton conduction and chemical reaction

• **Membrane** (Nafion): \sim 100 μ m

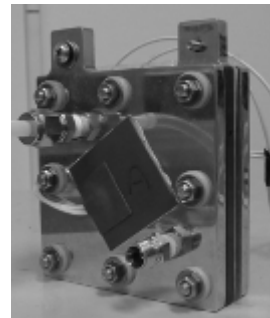
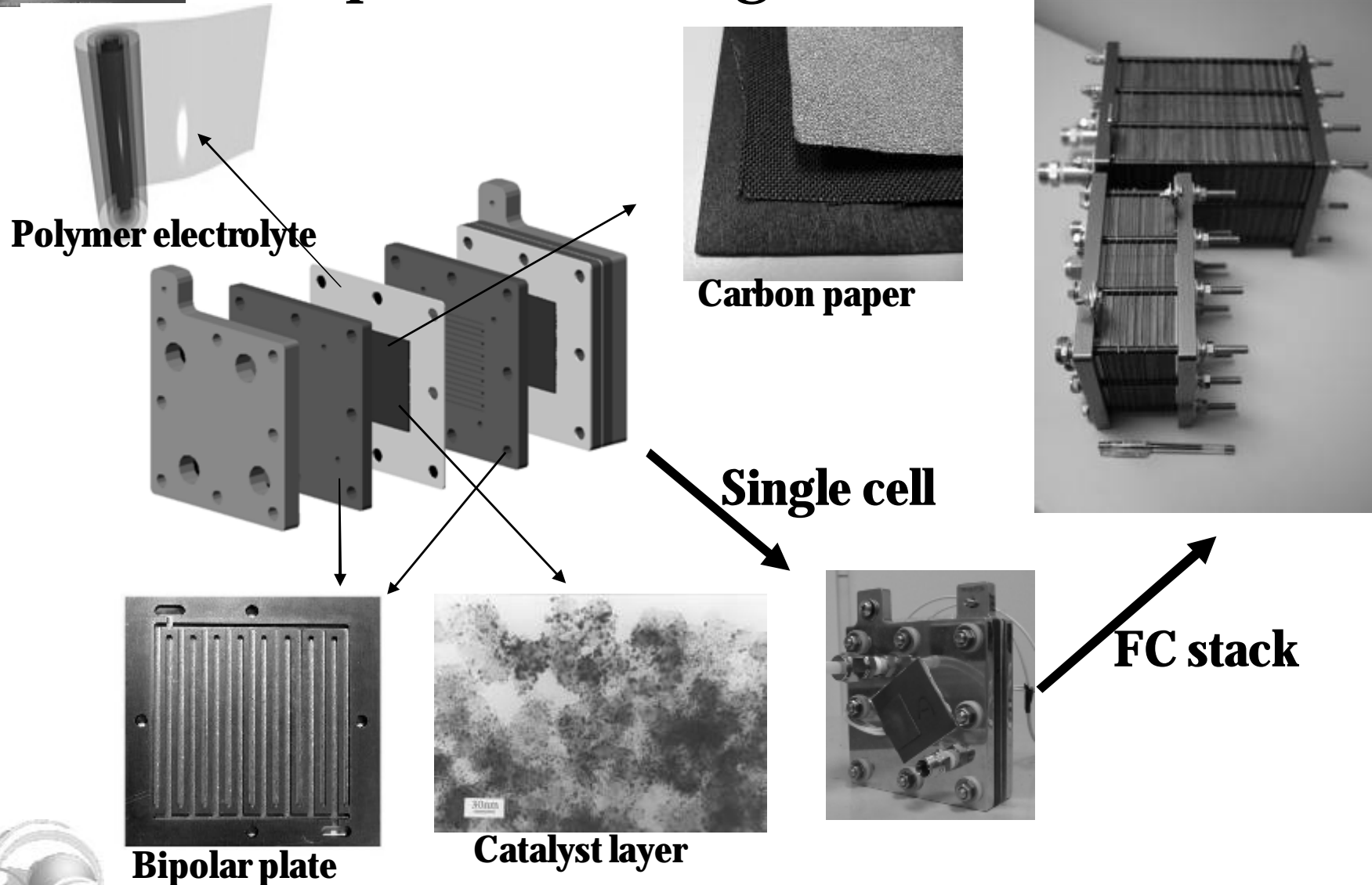
proton conduction and water transport

Over all: $H_2 + O_2 \rightarrow H_2O$



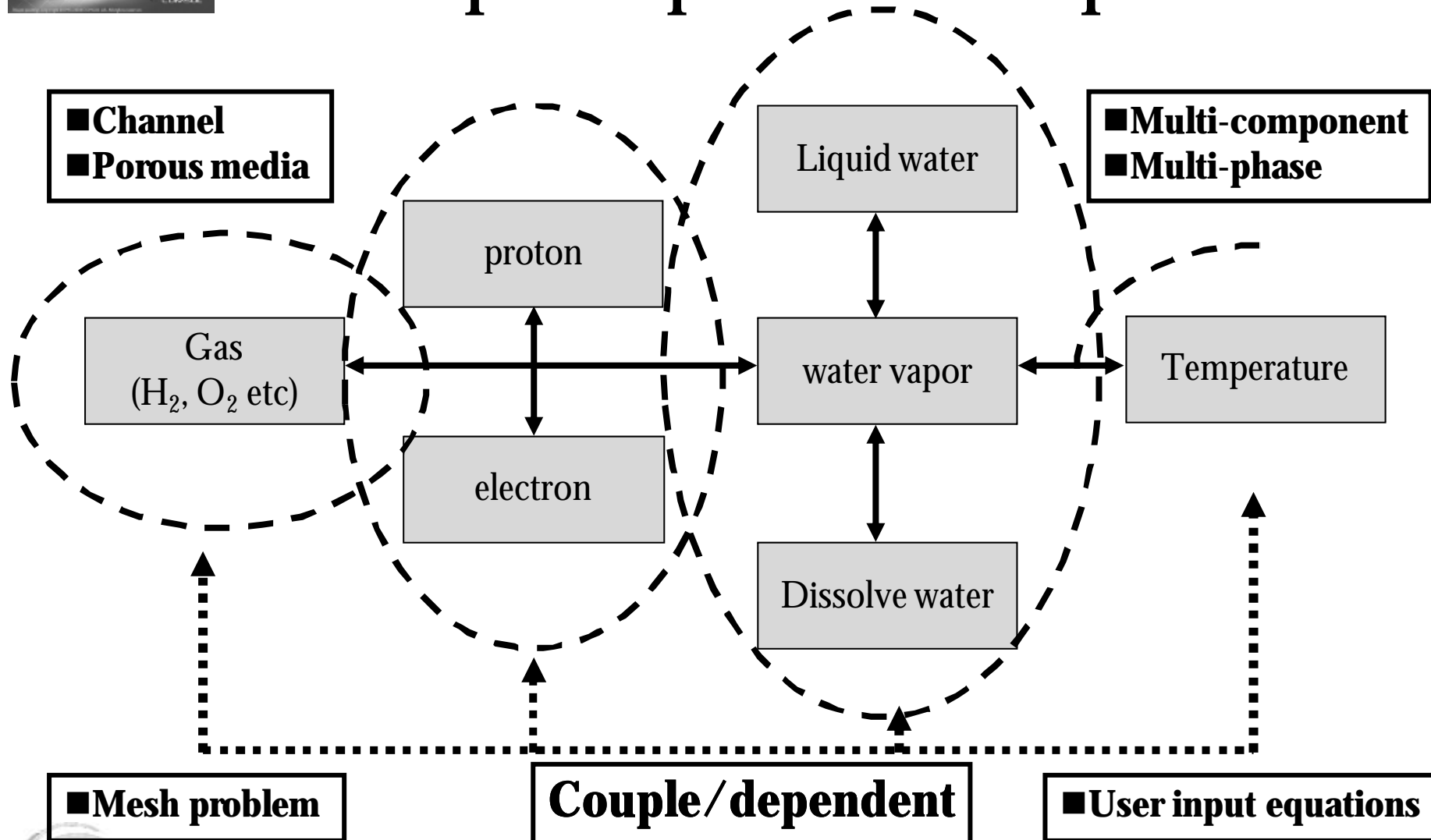


Components, single cell and stack





Complex species transport





Governing equations

- Conservation of species:

$$\nabla(-D_{\text{eff,O2}} \nabla C_{\text{O2}}) = S_{\text{O2}}$$

$$\nabla(-D_{\text{eff,H2}} \nabla C_{\text{H2}}) = S_{\text{H2}}$$

$$\nabla(-D_{\text{eff,wv}} \nabla C_{\text{wv}}) = S_{\text{wv}}$$

$$\nabla\left(-\frac{\mathbf{r}_{\text{nafion}}}{EW} D_{\text{H2O,eff}}^{\text{Naf}} \nabla I\right) - \nabla\left(\frac{n_d}{F} \mathbf{s}_p^{\text{eff}} \nabla \mathbf{f}_{\text{electrolyte}}\right) = S_I$$

$$\nabla(-\mathbf{r}_l D_{\text{cap}} \nabla s) - \nabla\left(\mathbf{r}_l \frac{k_{p,l}}{\mathbf{m}_l} \nabla p_g\right) = S_l$$

- Conservation of energy:

$$\nabla(-k_{\text{eff}} \nabla T) = S_T$$

- Conservation of potential:

$$-\nabla\left(\mathbf{s}_e^{\text{eff}} \nabla \mathbf{j}_{\text{Solid}}\right) = S_e$$

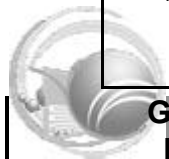
$$-\nabla\left(\mathbf{s}_p^{\text{eff}} \nabla \mathbf{j}_{\text{electrolyte}}\right) = S_p$$





Source terms

Source Terms	AGDL	ACL	PEM	CCL	CGDL
S_{O_2} mol/(m ³ s)				$j_c / 4F$	0
S_{H_2} mol/(m ³ s)	0	$-j_a / 2F$			
S_{wv} mol/(m ³ s)	$-S_l / M_{H_2O}$	$-S_l / M_{H_2O} - S_l$		$-S_l / M_{H_2O}$	$-S_l / M_{H_2O}$
$S_?$ mol/(m ³ s)		$\mathbf{x}_a \frac{\mathbf{r}_M}{EW} (\mathbf{I}_{eq} - \mathbf{I})$	0	$\mathbf{x}_a \frac{\mathbf{r}_M}{EW} (\mathbf{I}_{eq} - \mathbf{I})$	
S_l (kg/m ³ s)	S_l	S_l		$S_l - S_l M_{H_2O} - \frac{j_c}{4F} M_{H_2O}$	S_l
S_e (A/m ³)	0	$-j_a$		$-j_c$	0
S_p (A/m ³)		j_a	0	j_c	
S_T (W/m ³)	$\frac{I^2}{\mathbf{s}_e^{eff}} + S_l \Delta h_{lg}$	$ j \mathbf{h} + \frac{I^2}{\mathbf{s}_{eff}} + S_l \Delta h_{lg}$	$\frac{I^2}{\mathbf{s}_p^{eff}}$	$ j (\mathbf{h} - \frac{T\Delta S}{nF}) + \frac{I^2}{\mathbf{s}_{eff}} + S_l \Delta h_{lg}$	$\frac{I^2}{\mathbf{s}_e^{eff}} + S_l \Delta h_{lg}$





Transport parameters

$$D_{H_2}^0 = D_{H_2O}^0 = 1.055 \times 10^{-4} (T / 333)^{1.75} (101325 / P)$$

$$D_{H_2O}^0 = 0.2982 \times 10^{-4} (T / 333)^{1.75} (101325 / P)$$

$$D_{O_2}^0 = 0.2652 \times 10^{-4} (T / 333)^{1.75} (101325 / P)$$

$$D_{O_2, \text{nafion}}^0 = 3.1 \times 10^{-7} \exp(-2768 / T)$$

$$D_{H_2O, \text{nafion}}^0 = 3.1 \times 10^{-7} I (e^{0.28I} - 1) e^{(-2436 / T)} \quad 0 < I < 3$$

$$D_{H_2O, \text{nafion}}^0 = 4.17 \times 10^{-8} I (161e^{-I} + 1) e^{(-2436 / T)} \quad 3 \leq I \leq 17$$

$$H_{O_2}^{\text{Nafion}} = 1.33 \times 10^5 \exp(-666 / T)$$

$$s_p^0 = (0.514I - 0.326) \exp(1268(\frac{1}{303} - \frac{1}{T})) \quad I \geq 1$$

$$s_p^0 = 0.1879I \exp(1268(\frac{1}{303} - \frac{1}{T})) \quad I < 1$$





Kinetic parameters

$$\mathbf{h} = \mathbf{j}_{solid} - \mathbf{j}_{electrolyte} - \mathbf{j}_0$$

$$j_{0,a}^{ref} = i_{0,a}^{ref} \Big|_{343K} (S/V)_0 \exp \left[\frac{E_a^{act}}{R} \left(\frac{1}{343} - \frac{1}{T} \right) \right]$$

$$j_{0,c}^{ref} = i_{0,c}^{ref} \Big|_{343K} (S/V)_0 \exp \left[\frac{E_c^{act}}{R} \left(\frac{1}{343} - \frac{1}{T} \right) \right]$$

$$j_a = j_{0,a}^{ref} \left(\frac{P_{H2}}{P_{H2}^{ref}} \right) \left[\exp \left(\frac{a h F}{RT} \right) - \exp \left(- \frac{a h F}{RT} \right) \right]$$

$$j_c = -4F \frac{P_{O2}}{H_{O2}^{Naf}} \mathbf{x} k_h$$

$$\mathbf{f} = \frac{r_{agg}}{3} \sqrt{k_h / [D_{O2,eff}^{eff} (1 - \mathbf{e}_{CL})]}$$

$$\mathbf{x} = [3\mathbf{f} \coth(3\mathbf{f}) - 1] / (3\mathbf{f}^2)$$

$$k_h = \frac{1}{4FC_{O2}^{ref}} j_{0,c}^{ref} \exp \left[- \frac{a_c h F}{RT} \right]$$

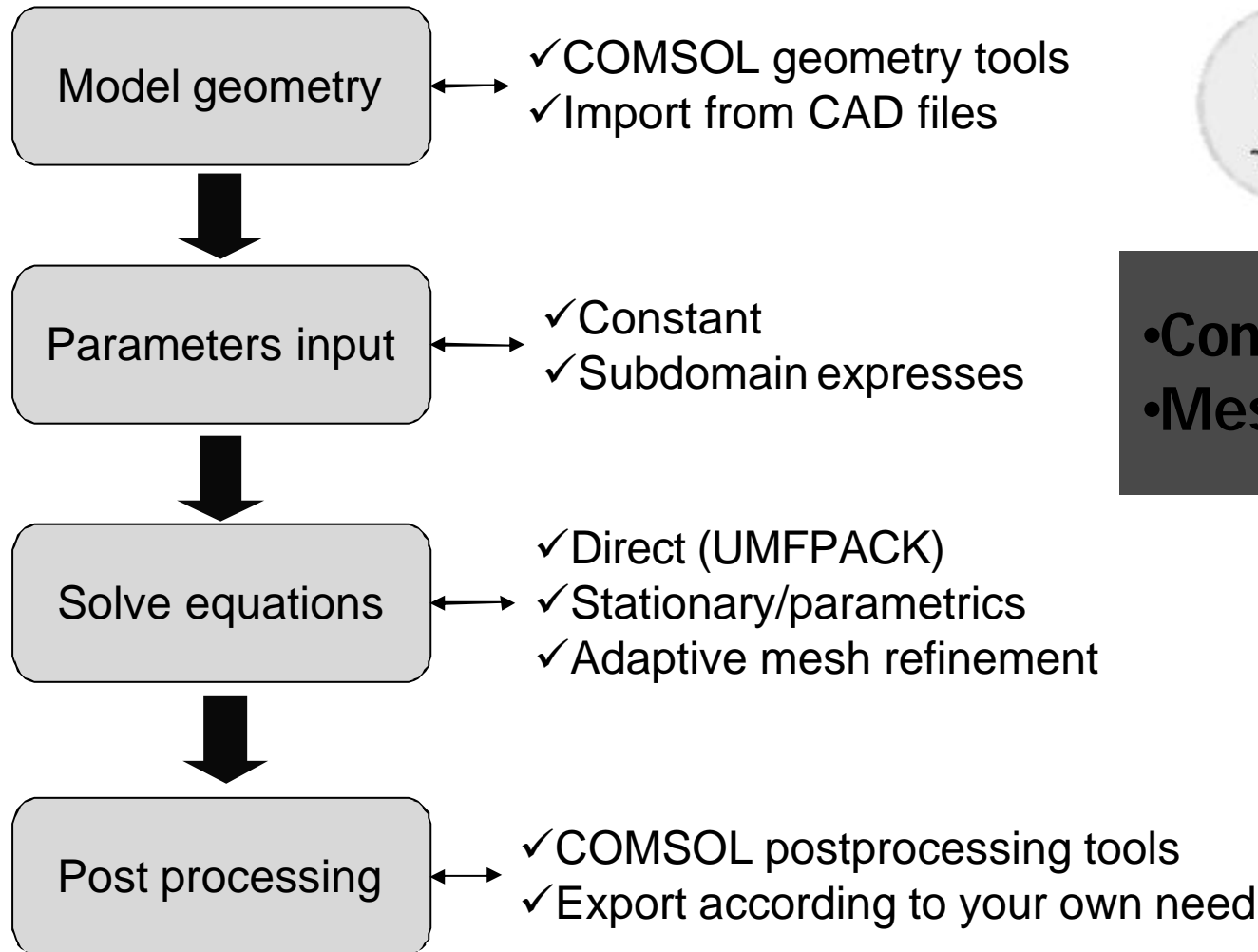
$$S_l = K_{cond} \Delta P \mathbf{e} s \mathbf{r}_l : \Delta P < 0$$

$$S_l = K_{cond} \Delta P \frac{\mathbf{e} (1-s) X_{wv} M_{H2O}}{RT} : \Delta P \geq 0$$





Simulation flow chart



•Convergence
•Mesh





Challenges & solutions

- Convergence
 - Mainly due to coupled equations (8) and lots of variable dependent parameters.
 - ✓ Appropriate value of initial value
 - ✓ Using RESTART to solve equations step by step
- Mesh
 - Finer or coarser mesh are both possible to solve the problem





Models used in COMSOL

- Chemical Engineering Module
 - Mass Transport → Convection and Diffusion (4)
 - Energy Transport → Convection and Conduction(1)
- AC/DC Module
 - Conductive Media DC (2)
- COMSOL Multiphysics Module
 - PDE, Coefficient Form(1)

All solved variables are dependent





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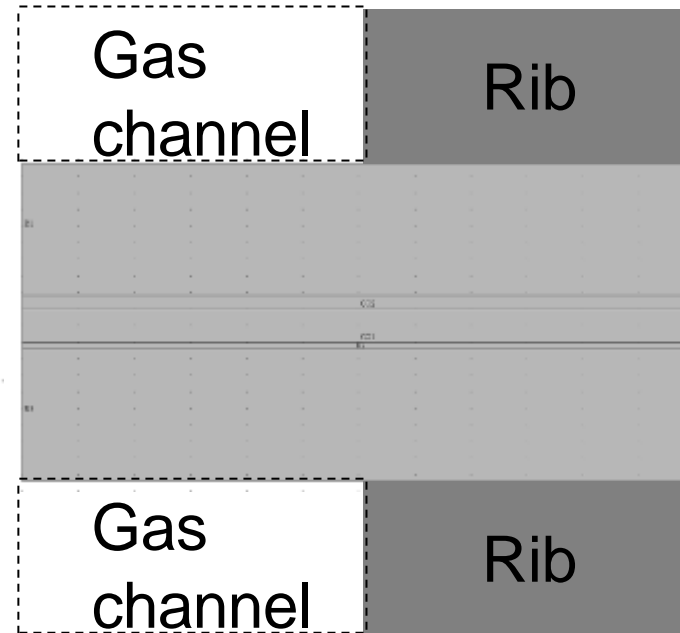
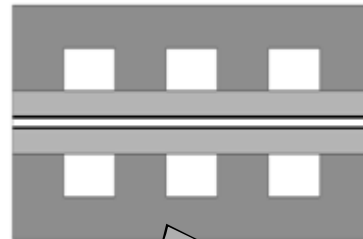
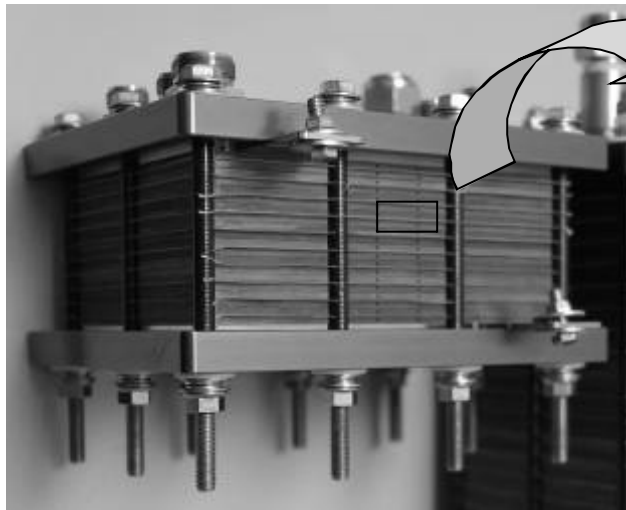
Examples solved by COMSOL - PEMFC & SOFC





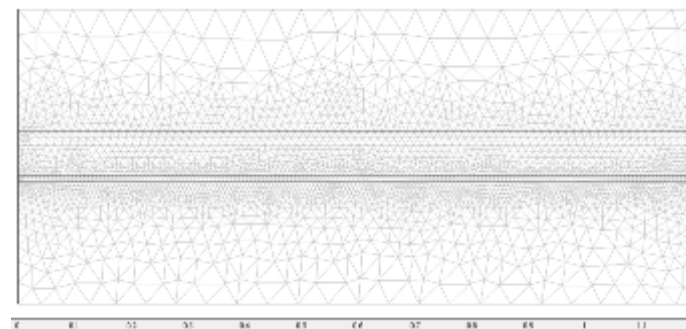
2D simulations

- Simulation domain



Cathode GDL: 200 μ m
Cathode CL: 20 μ m
Electrolyte: 50 μ m
Anode CL: 10 μ m
Anode GDL 200 μ m

Anode CL
Anode GDL



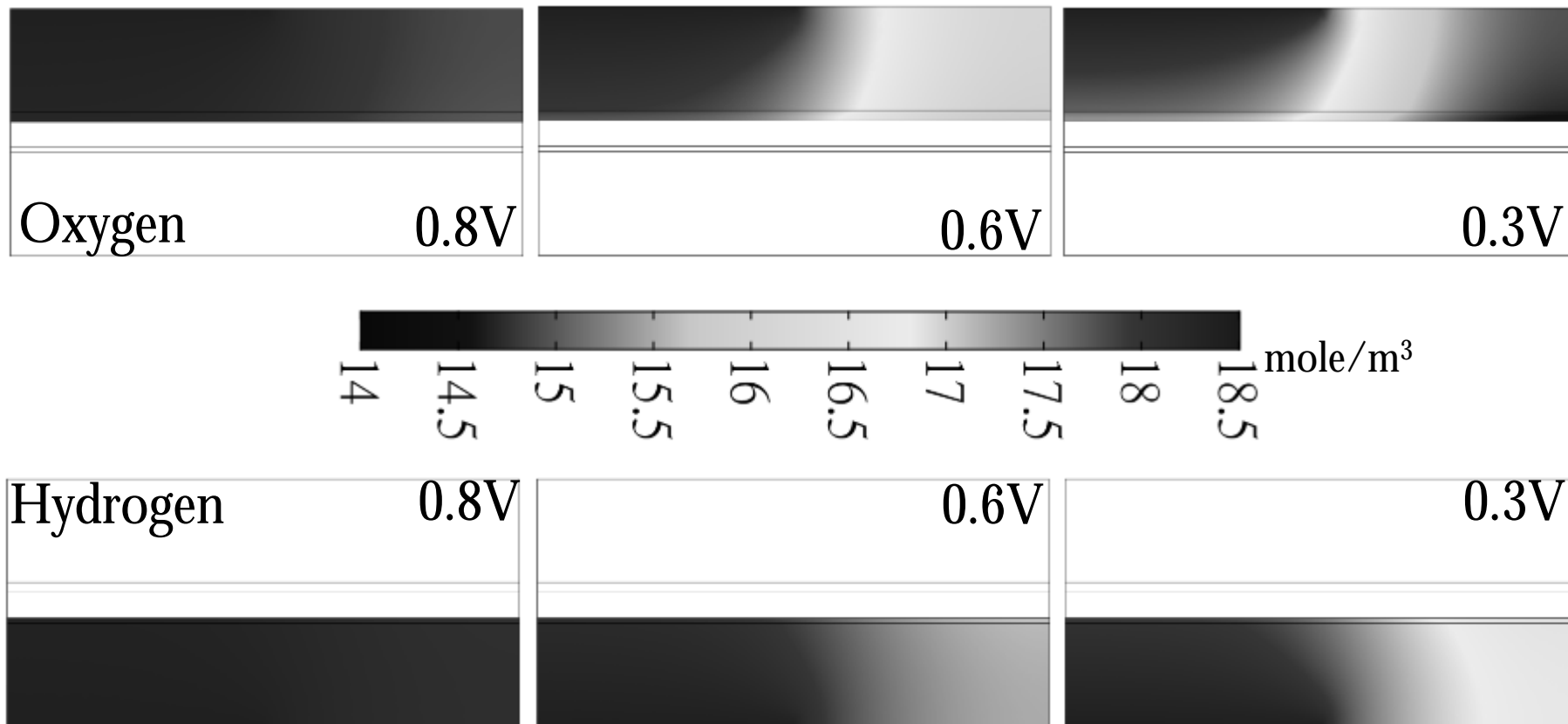
Cathode GDL
Cathode CL





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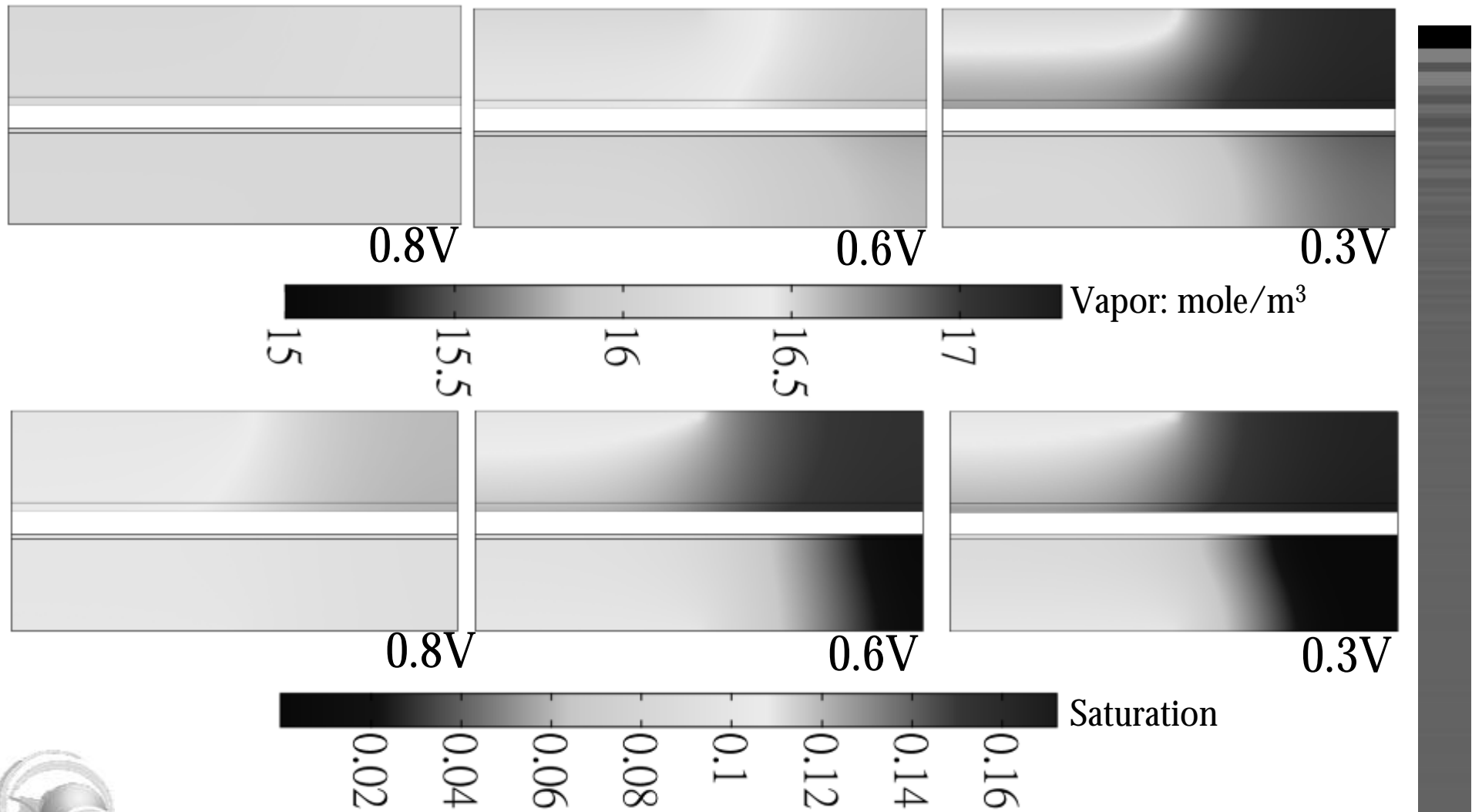
O₂/H₂ consumption





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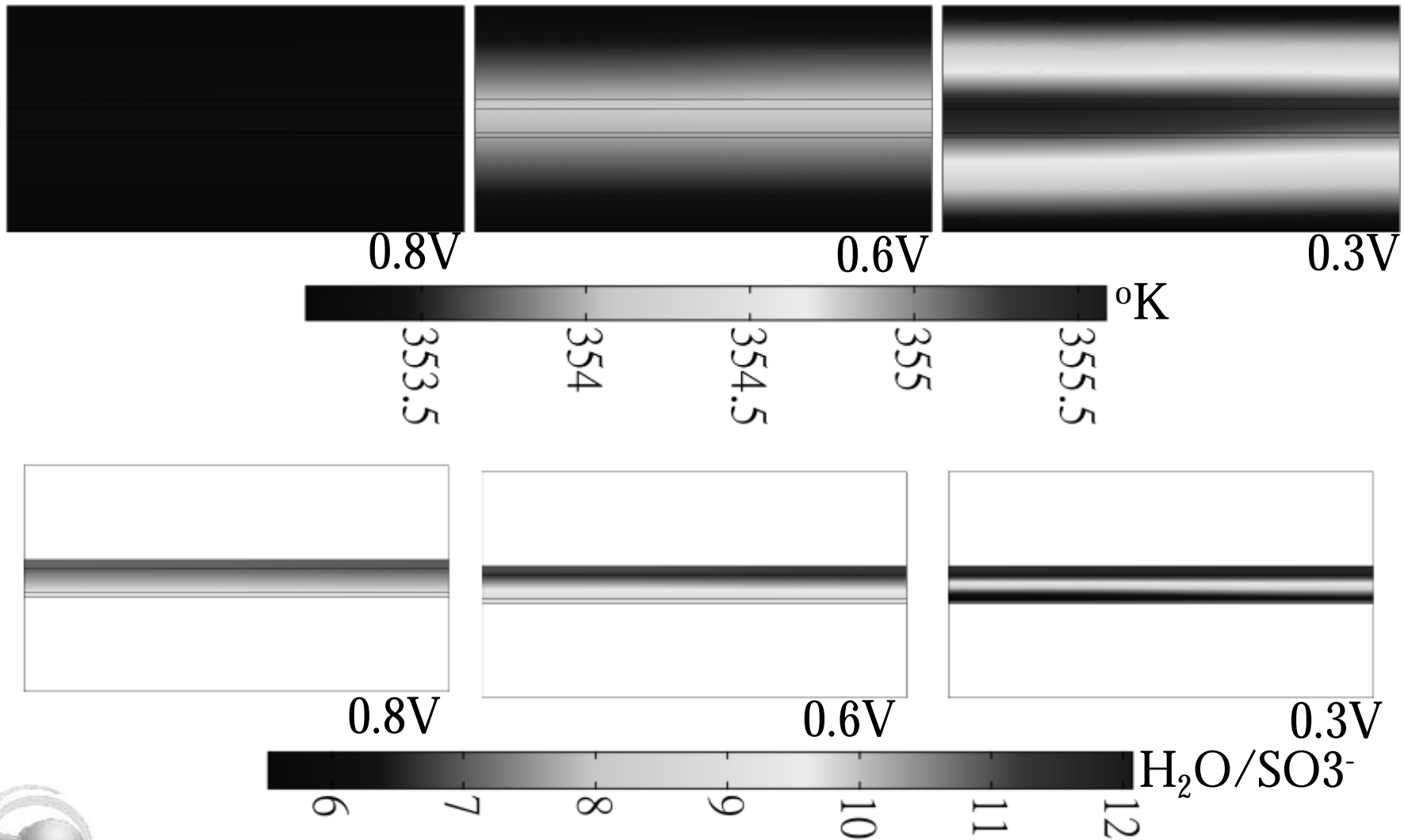
Water (vapor & liquid)





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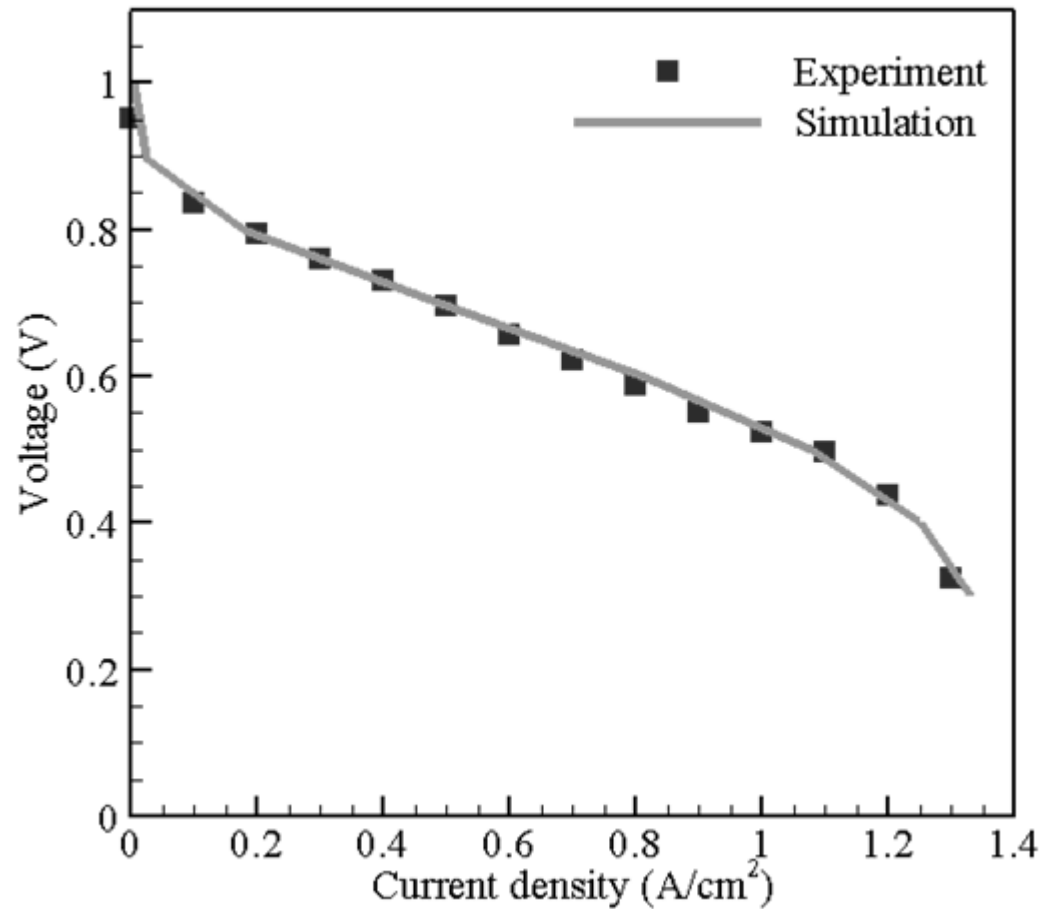
Temp./water content plot





Validation with exp

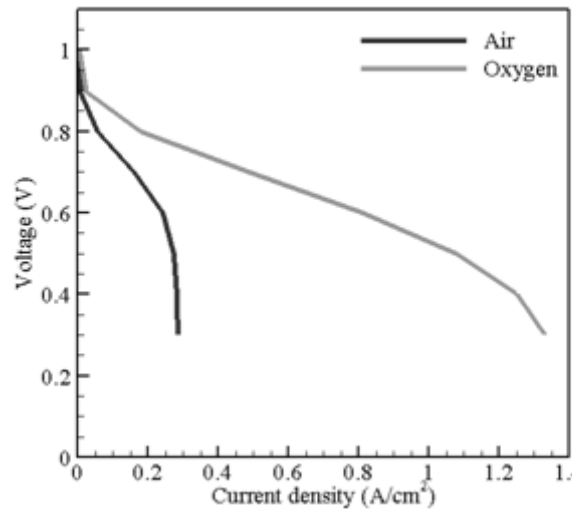
- ✓ Performance curve
- ✓ Operation condition
- ✓ Parameter sensitivity



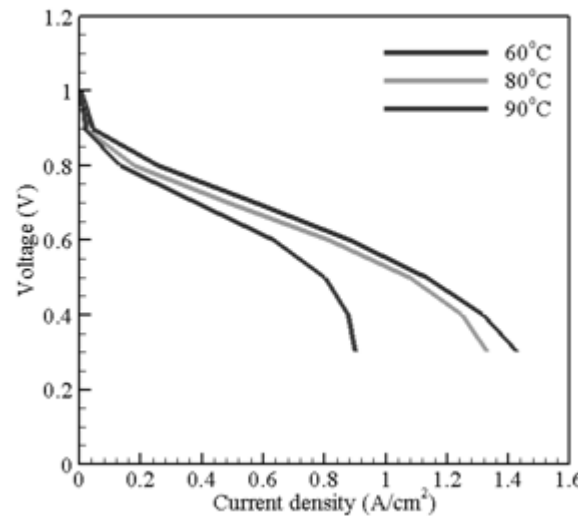


Operation conditions

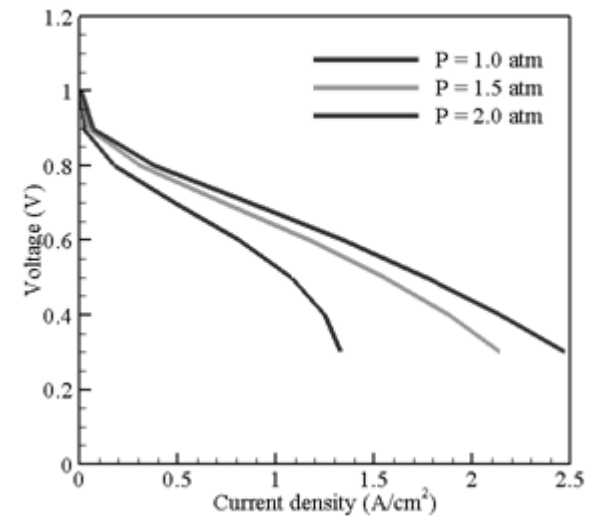
•O₂/Air



•Temperature effect

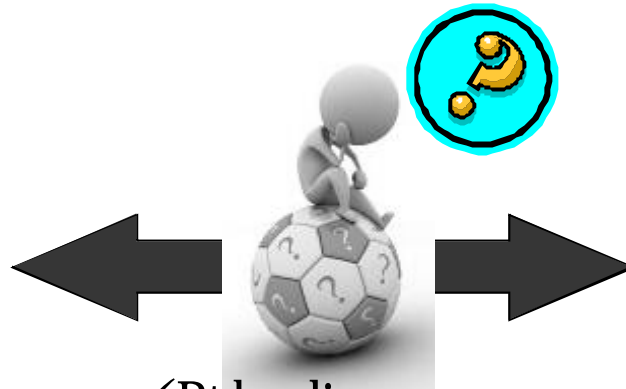


•Pressure effect





INCREASE
CL performance



REDUCE
CL cost

- ✓ Pt loading
- ✓ Nafion content
- ✓ Pt/C wt%
- ✓ Support material
- ✓ CL thickness
- ✓ Alternative catalyst material

CL with d

Perfo

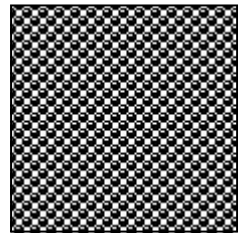
Cost can be reduced!



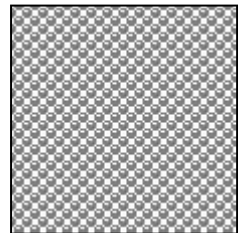


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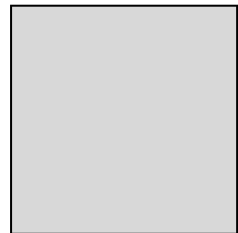
Different CL design



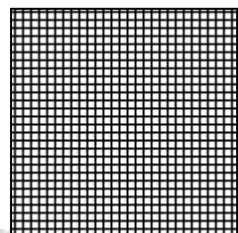
Pt/C: 80wt%



Pt/C: 40wt%

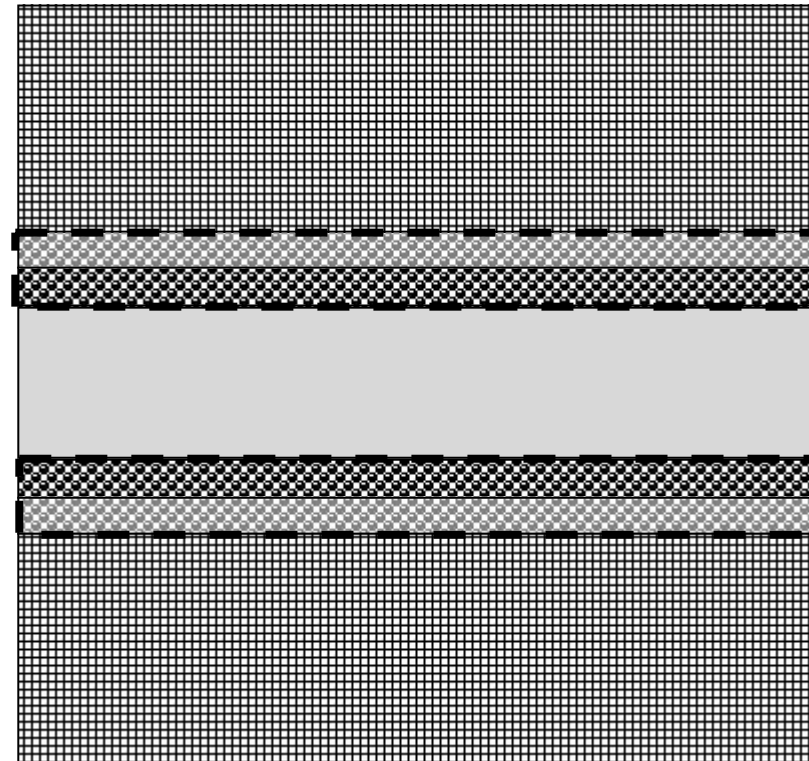


Mem(Nafion)



Gas diffusion layer

Non-uniform composition of Pt/C ratio



CGDL

CCL

MEM

ACL

AGDL

MEA structure





Case studied

•Cathode: 1.0 mg/cm²

MEA#	1	2	3	4
Pt/C 80wt	0	0.1	0.2	0.4
Pt/C 40wt	1.0	0.9	0.8	0.6
Total	1.0	1.0	1.0	1.0

unit: mg/cm²

•Anode: 0.5 mg/cm²

MEA#	1	2	3	4
Pt/C 80wt	0	0.05	0.1	0.2
Pt/C 40wt	0.5	0.45	0.4	0.3
Total	0.5	0.5	0.5	0.5

unit: mg/cm²

Content of Pt/C 80wt% increase?

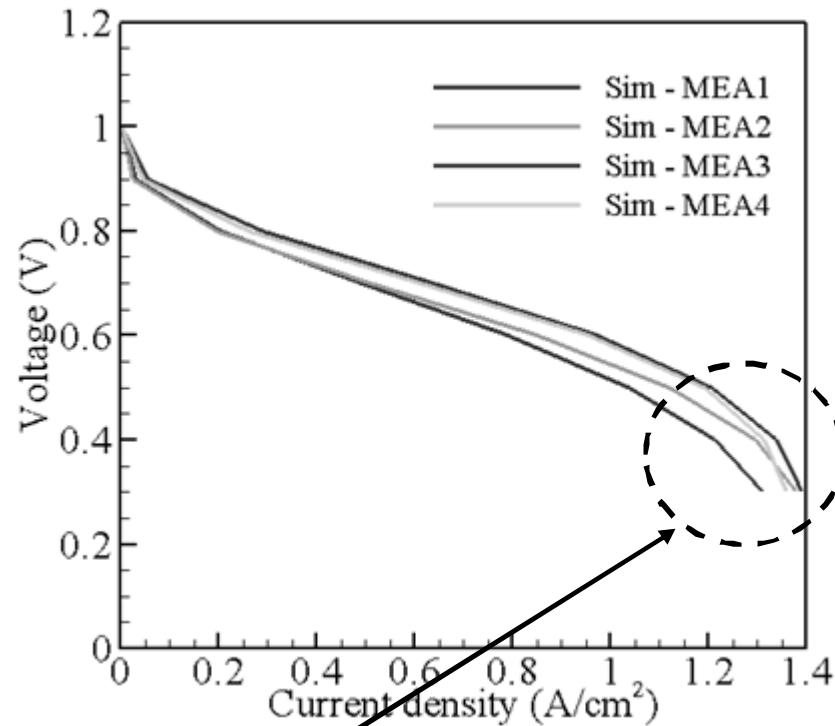
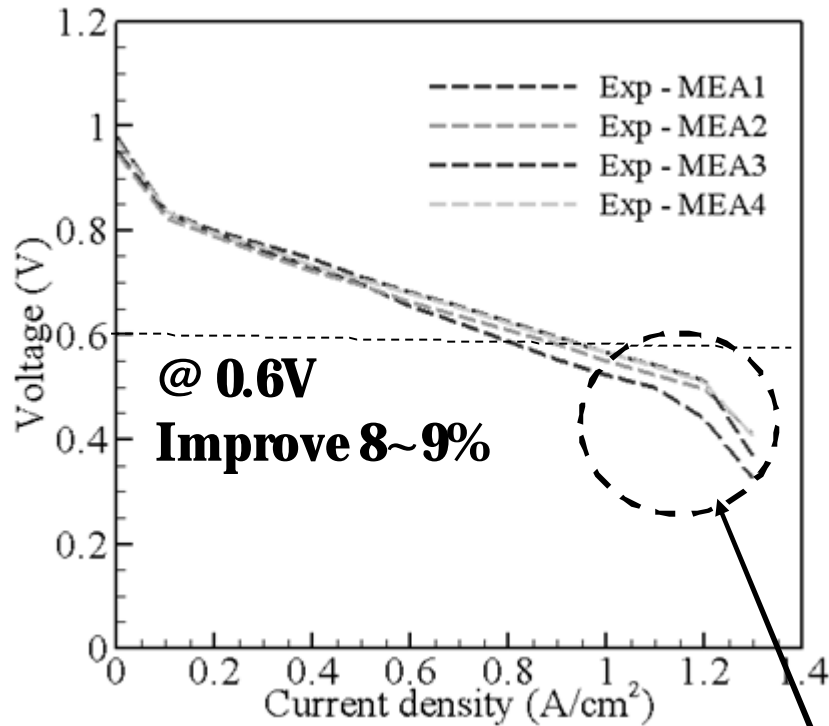




Experimental validation



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**Variation of the performance is reproduced!
Trend of mass transport limit region is reproduced!
MEA3>MEA4>MEA2>MEA1**





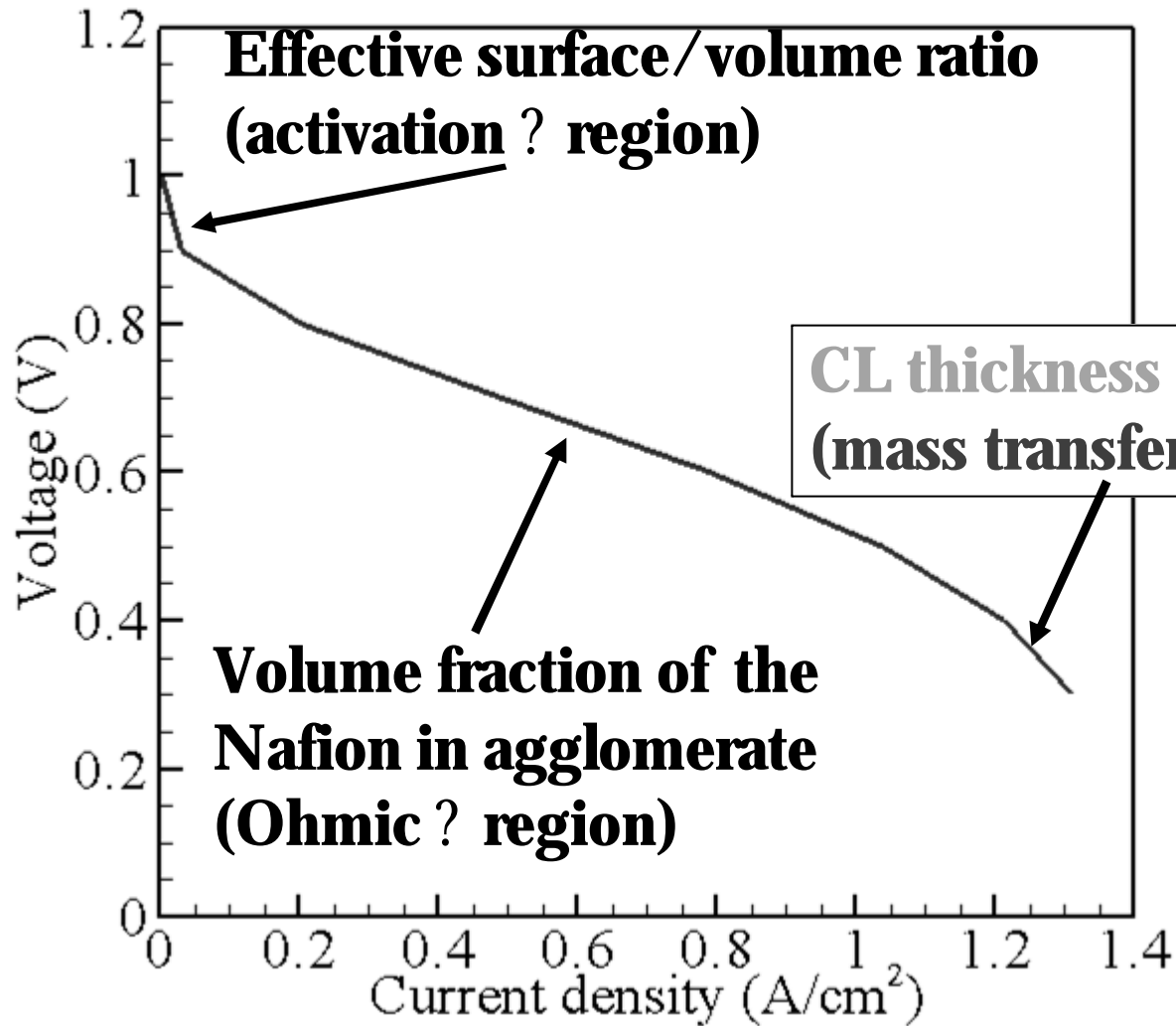
Key parameters in CL model

- When Pt/C wt% changes... ..
 - Porosity
 - **CL thickness**
 - **Volume fraction of the Nafion in agglomerate**
 - **Volume fraction of the Pt/C in agglomerate**
 - **Thickness of the Nafion cover on the agglomerate**
 - **Effective surface to volume ratio**



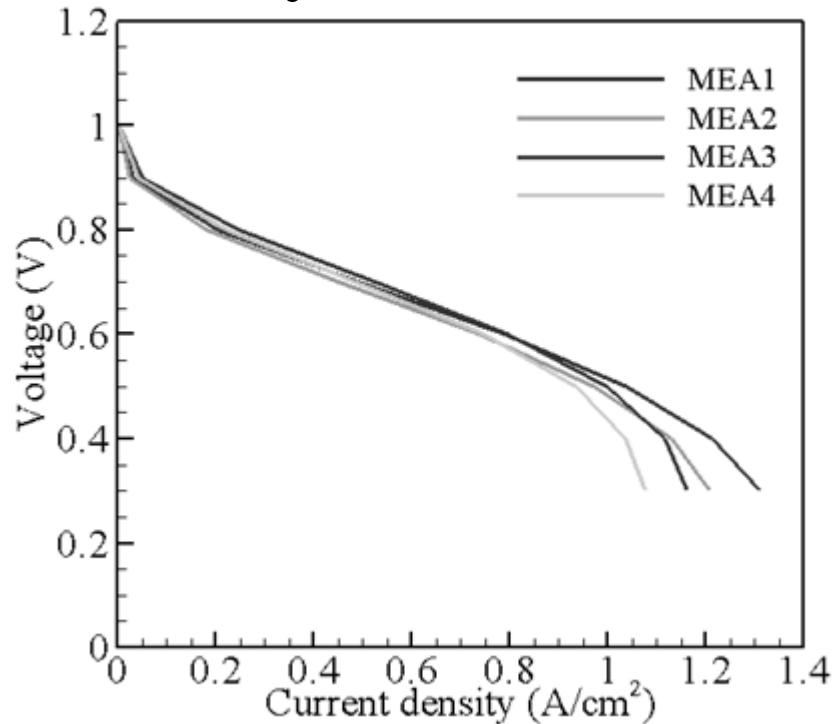


Dominant factors



Effects of different CL sub-layer

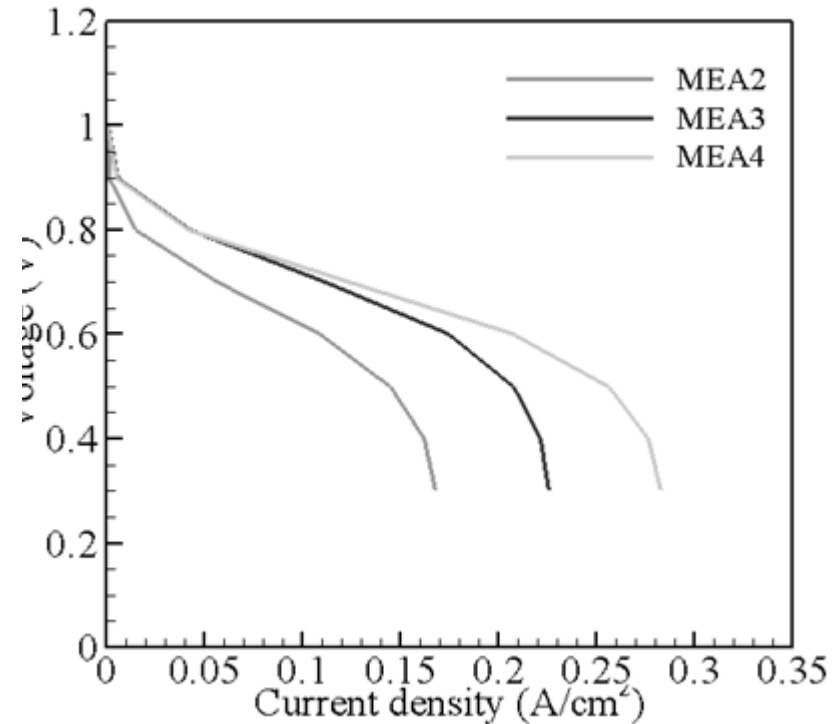
•Sub-layer with Pt/C 40wt%



MEA1 > MEA2 > MEA3 > MEA4

-0.1 -0.04 -0.09
A/cm² A/cm² A/cm²

•Sub-layer with Pt/C 80wt%



MEA1 < MEA2 < MEA3 < MEA4

+0.167 +0.057 +0.057
A/cm² A/cm² A/cm²



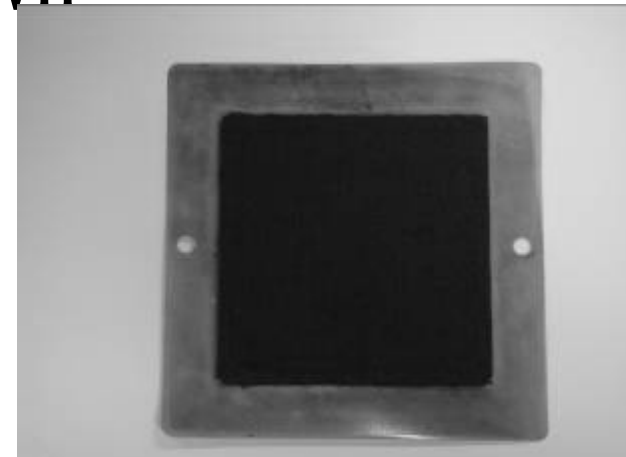


PBI based HT-PEMFC



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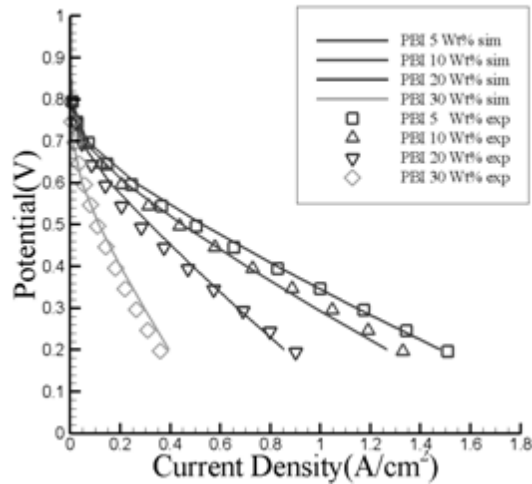
- Operation temperature can be raised to $\sim 180^{\circ}\text{C}$
- No water management is required
- Higher electrode kinetics
- Acid doping level is important
- Best CL composition is unknown



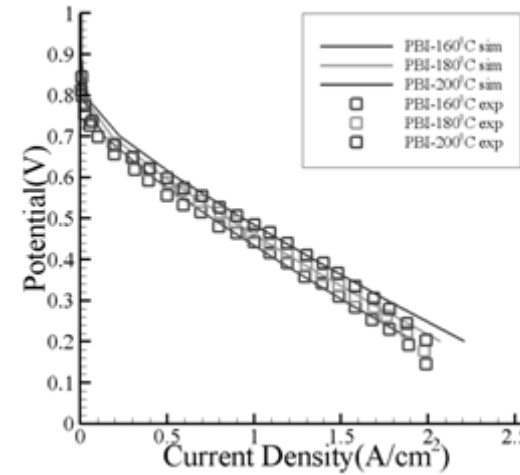


PBI wt% % Temp effect

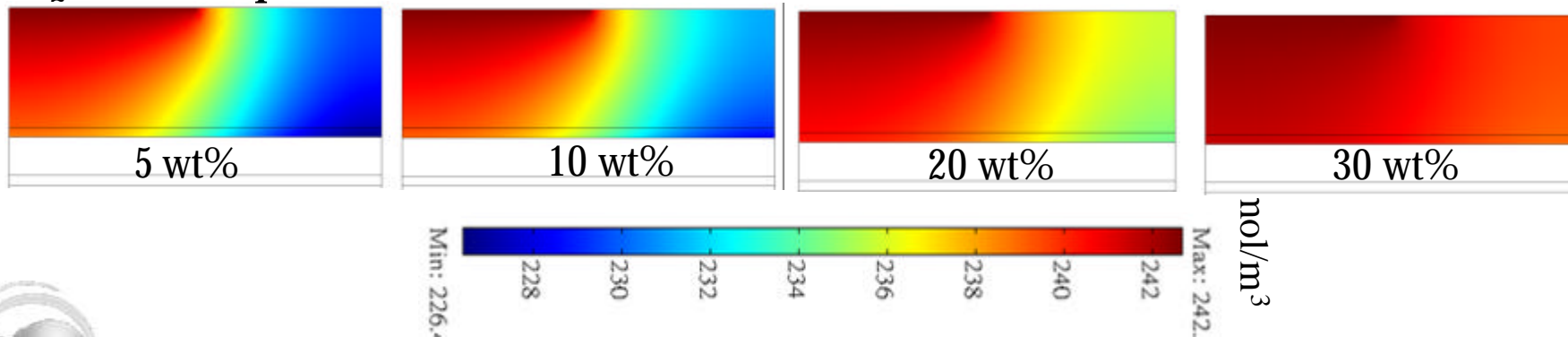
PBI wt% effect



Temperature effect

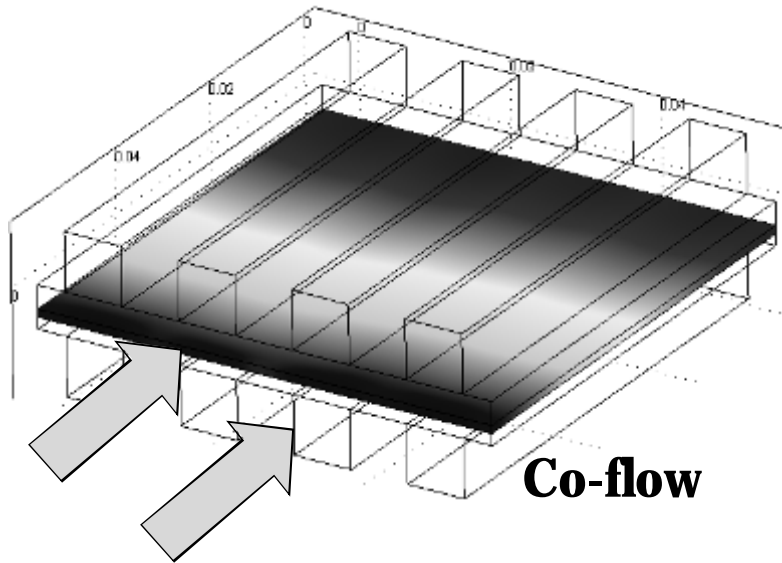


O₂ consumption

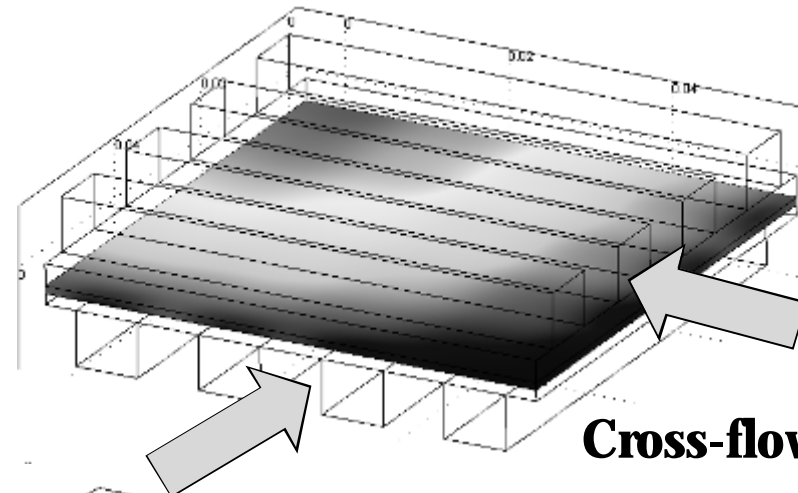




Temp. distribution

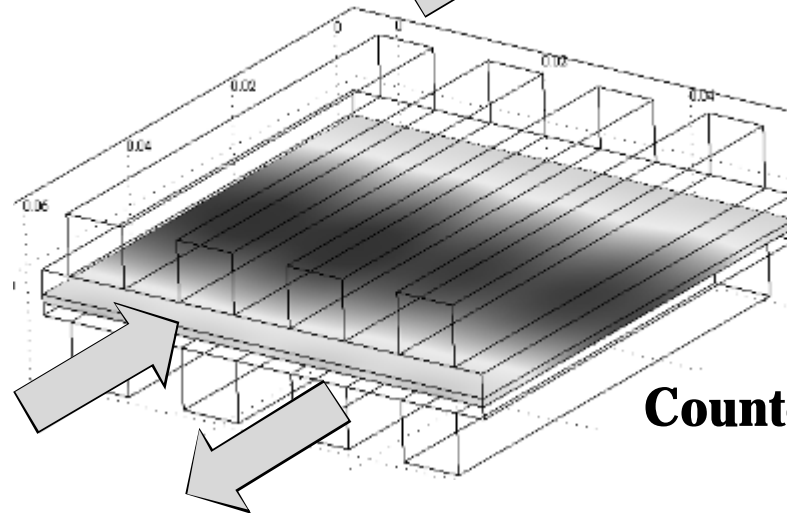


Co-flow



Cross-flow

Temperature distribution is highly non-uniform on the electrolyte

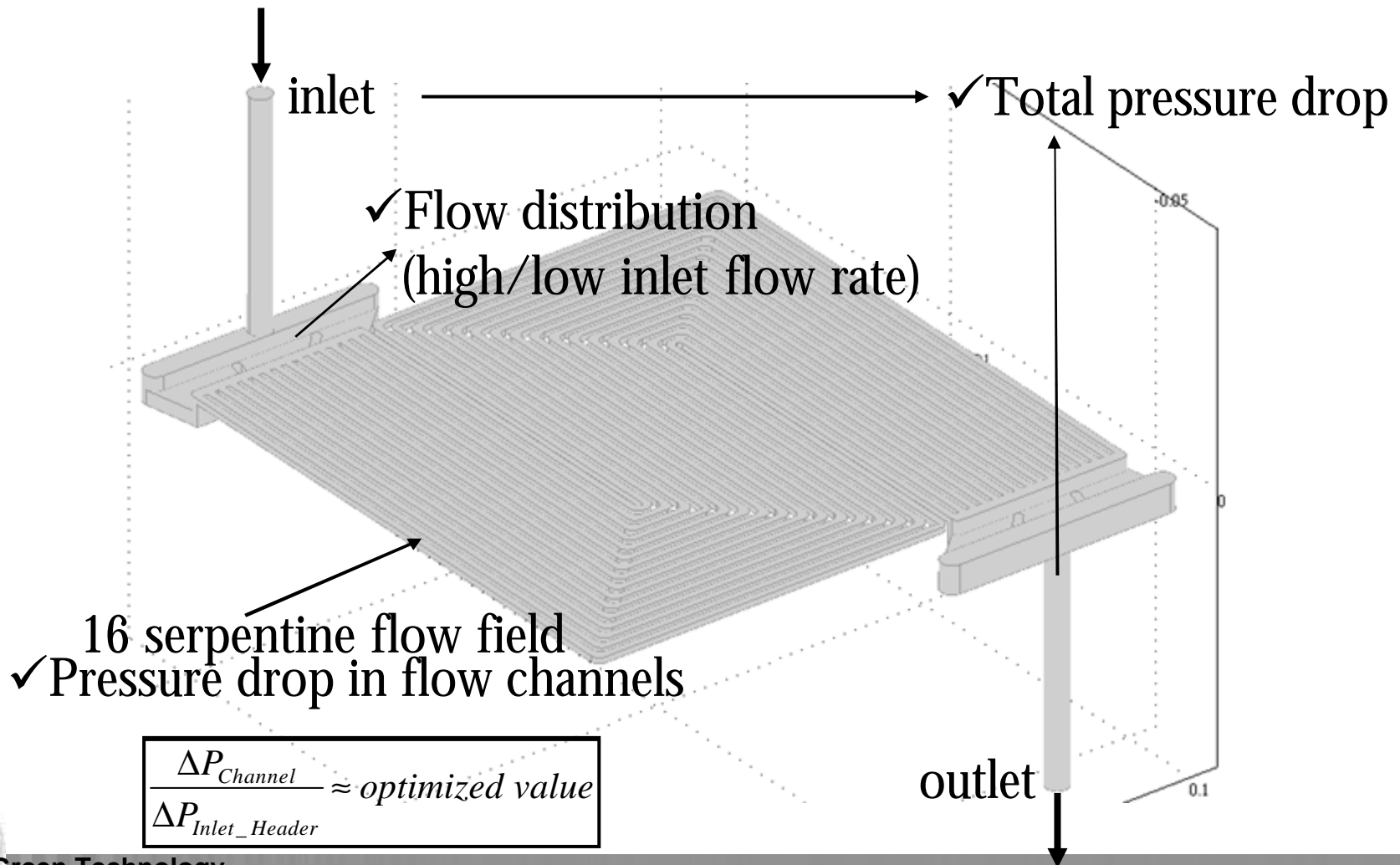


Counter-flow





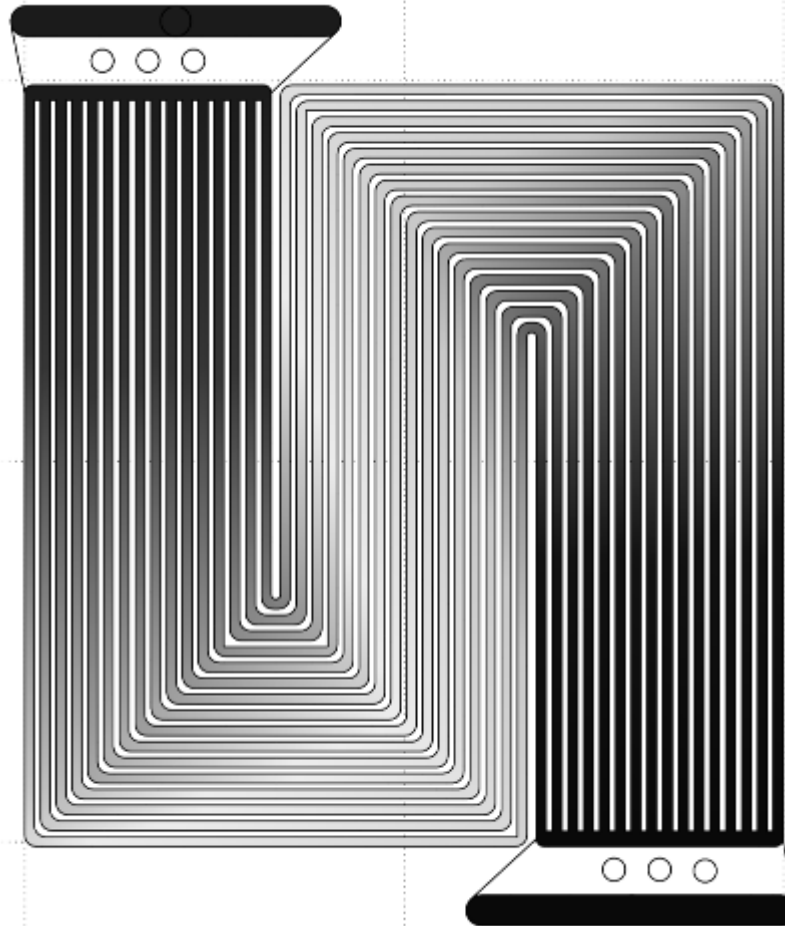
FC stack simulation



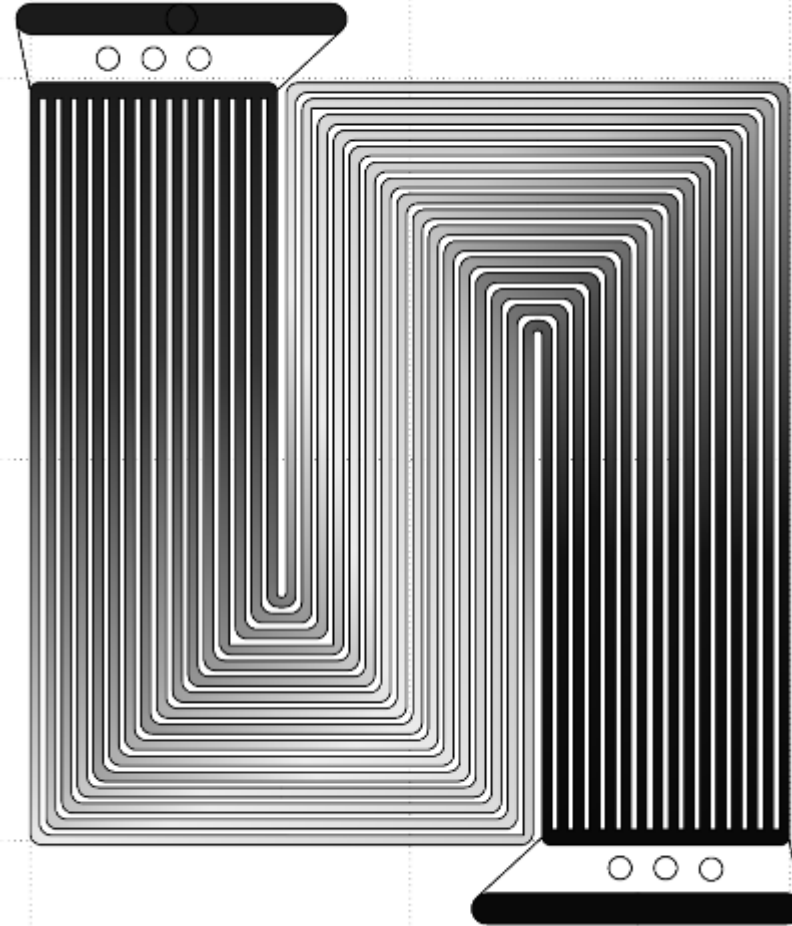


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Pressure drop



High flow rate $\Delta P \sim 155 Pa$



Low flow rate $\Delta P \sim 63 Pa$

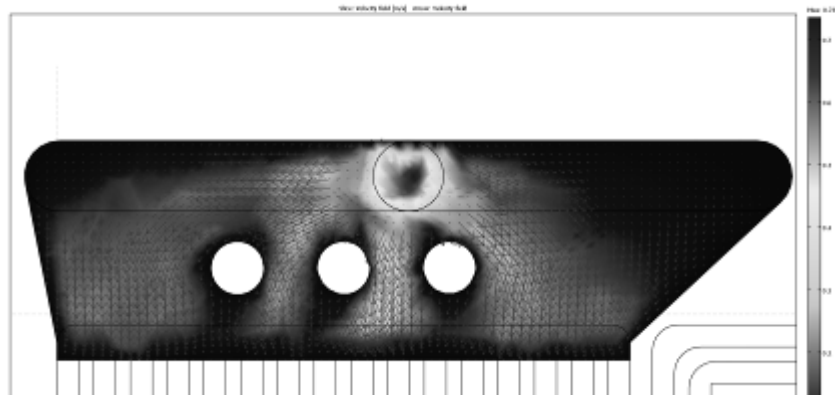




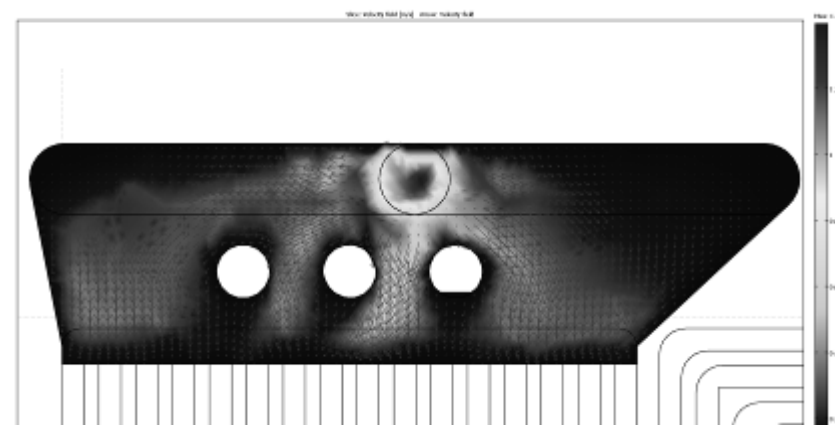
Flow distributor effect



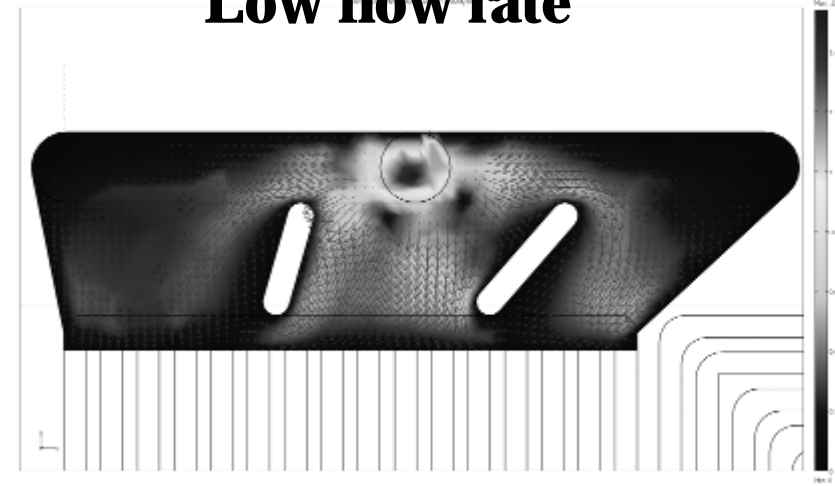
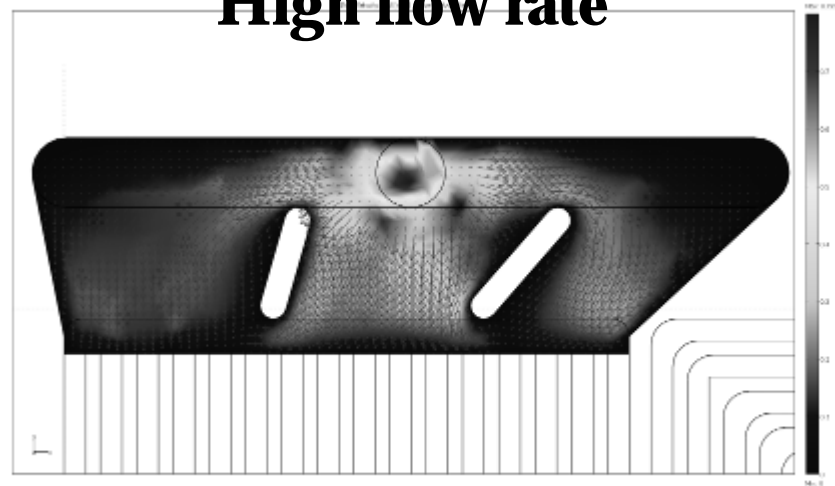
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High flow rate

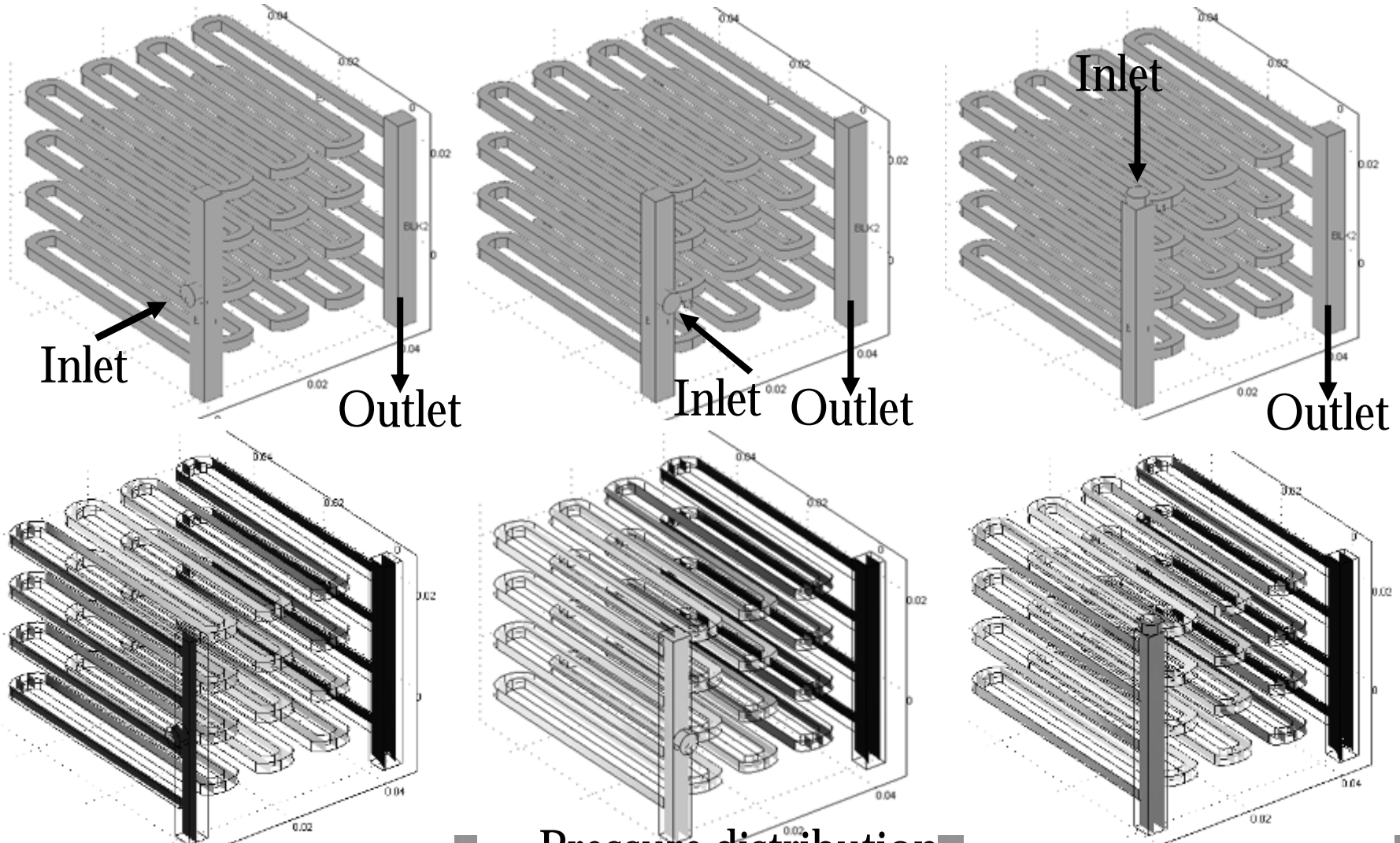


Low flow rate





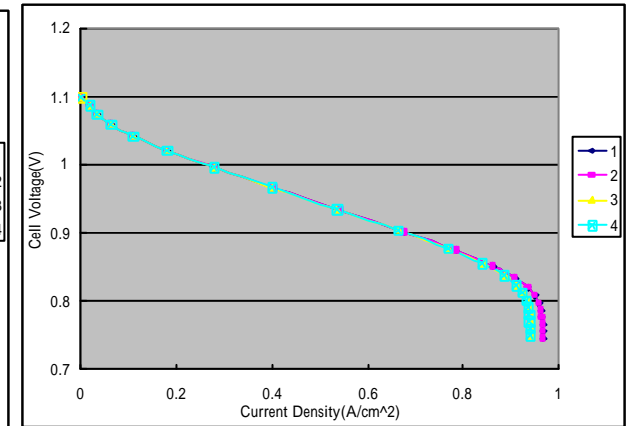
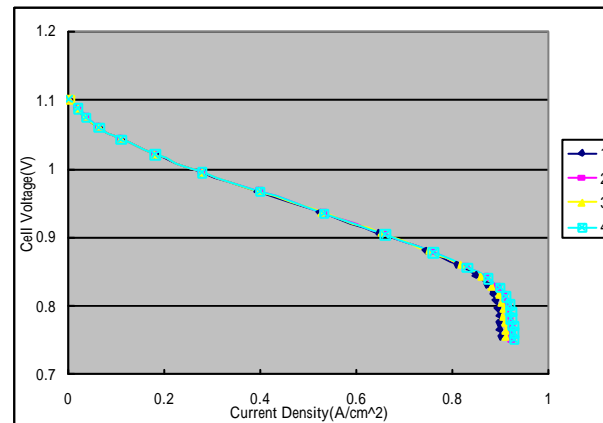
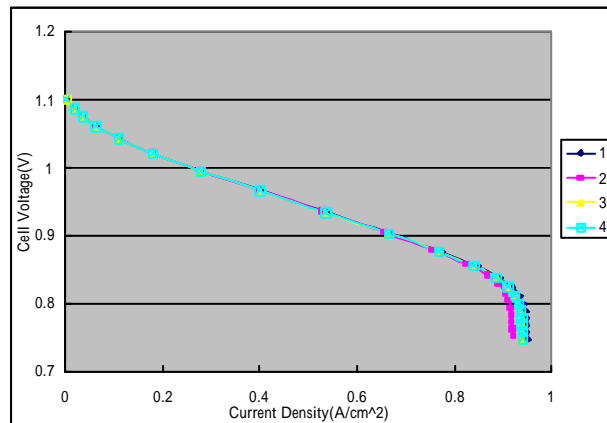
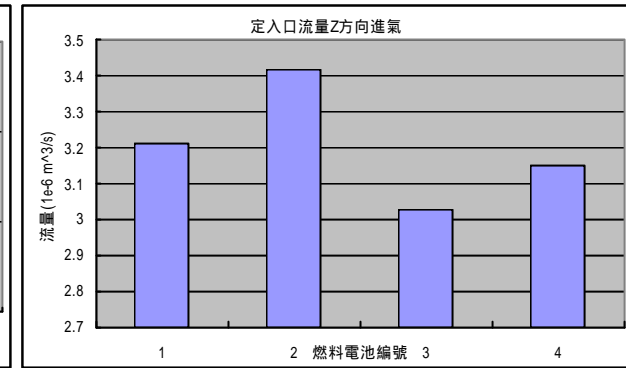
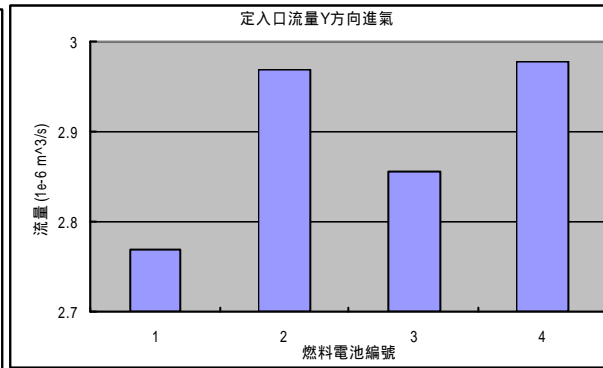
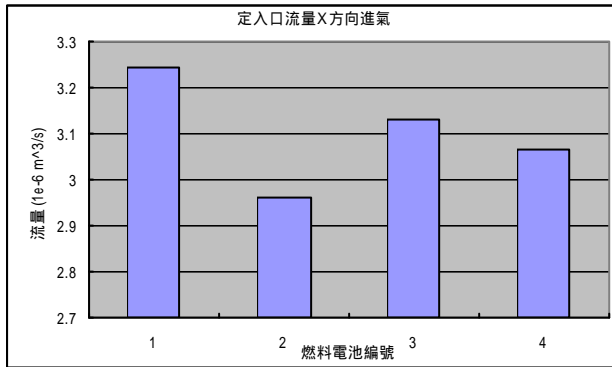
FC stack simulation



Pressure distribution Modeling & Simulation Lab



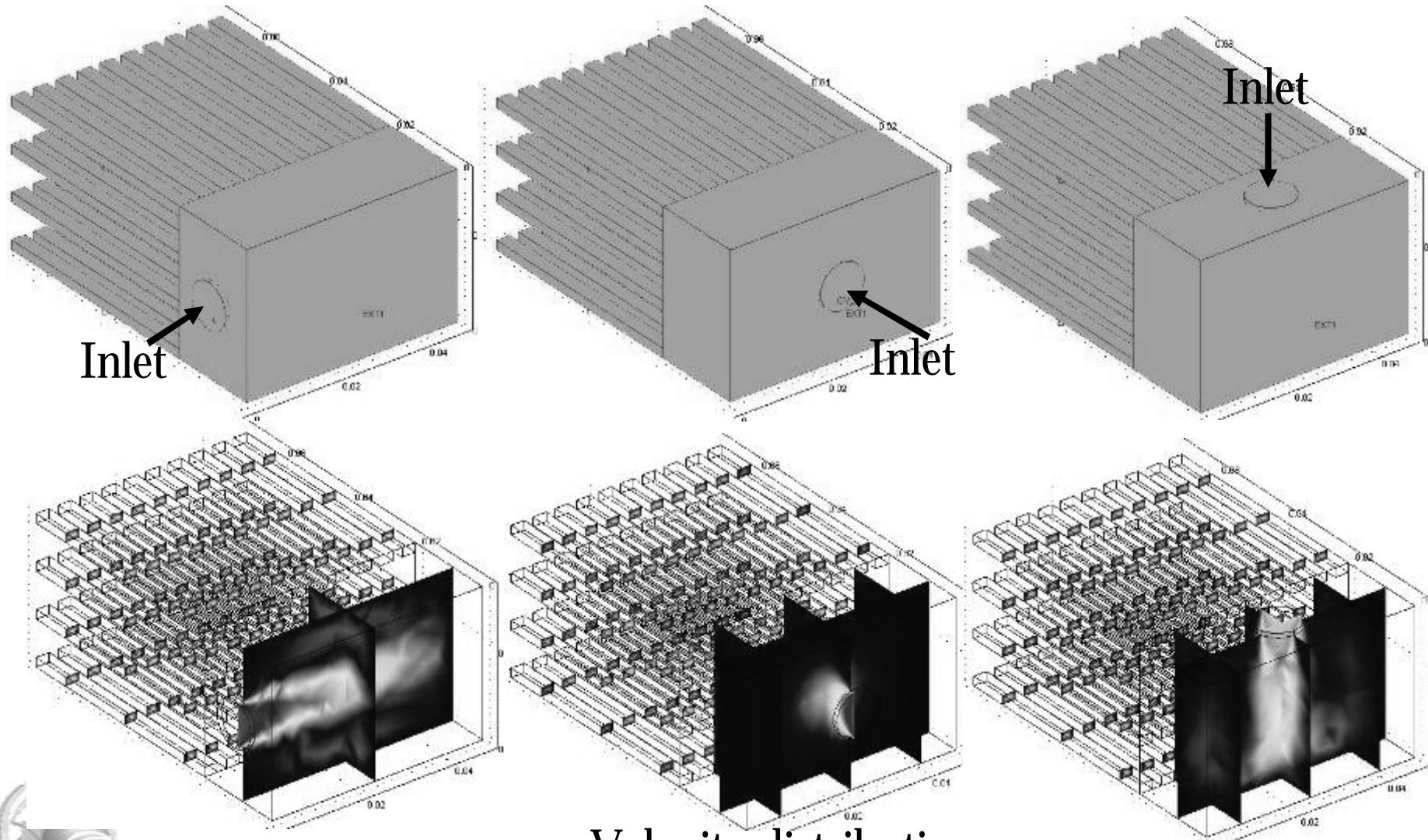
Flow distribution





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FC stack simulation



Velocity distribution

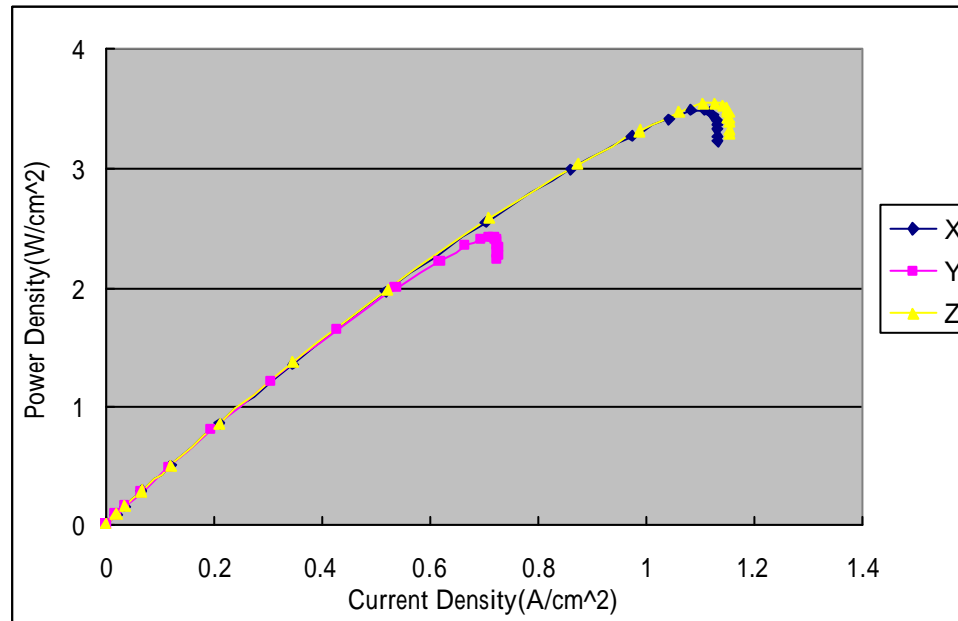
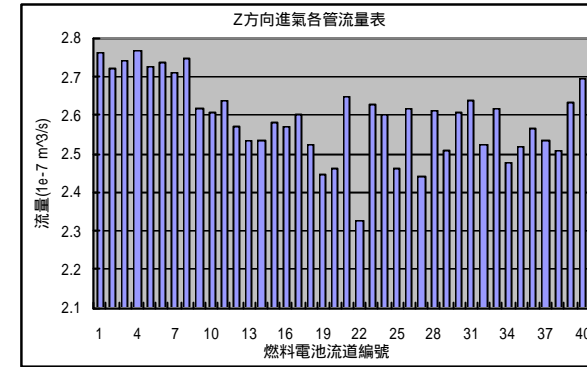
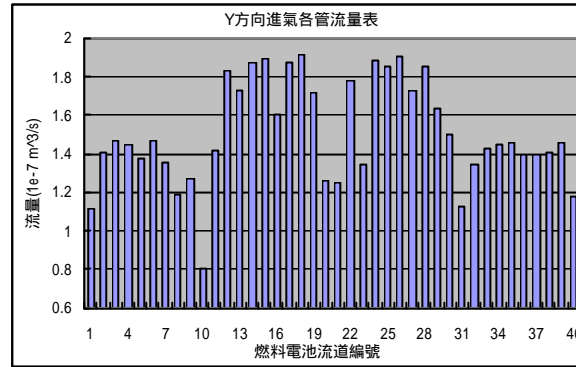
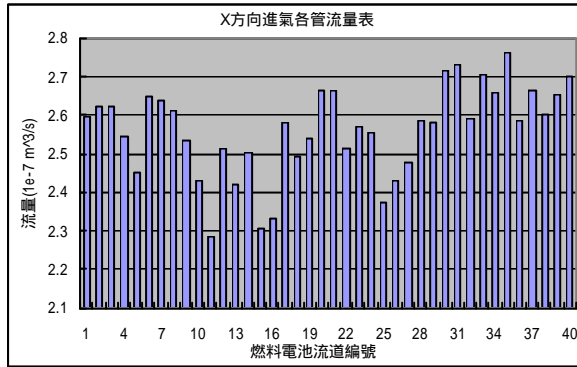
Modeling & Simulation Lab



Green Technology
Research Center

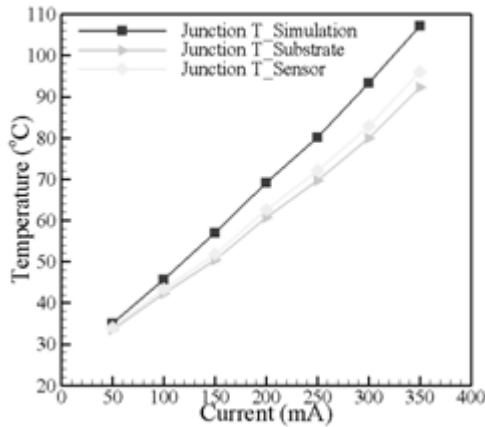
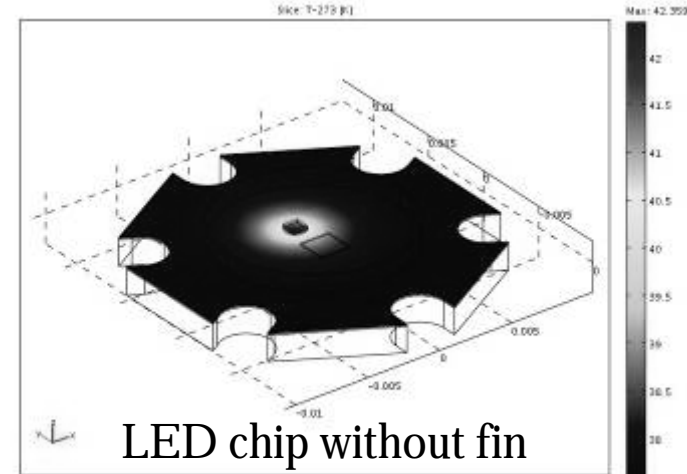
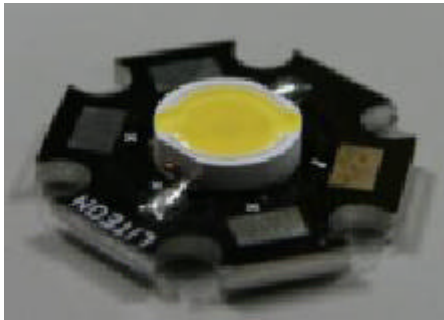


Flow distribution

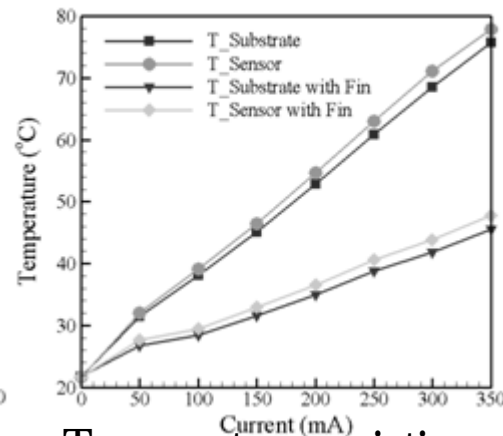




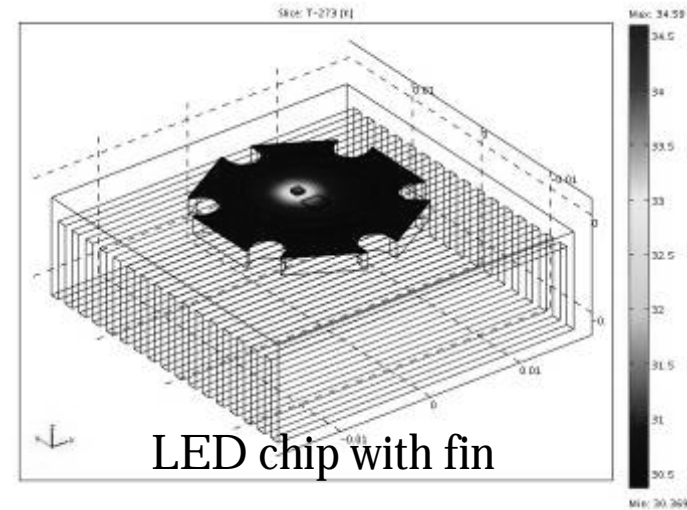
Heat transfer in LED



Junction temperatures at various current input



Temperature variation at different current input



LED chip with fin





Summary

- COMSOL Multiphysics is good at complex coupling problems
 - Different models can be integrated easily
 - Friendly user input interface
- It has been shown that modeling/simulation of fuel cells (component, single cell or stack) & LED is feasible.





Yuan-Ze University

Thanks for your attention!

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